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(54) PROCESS FOR REDUCING ALDEHYDES OR KETONES.

(57) A process for reducing aldehydes or ketones using a stable and highly active catalyst not soluble in a solvent, easily removable from the reaction system after completion of the reaction, and reusable. This process comprises reacting an aldehyde or a ketone with an alcohol using zirconium oxide hydrate as a catalyst.

DESCRIPTION

1. Title of the Invention:

PROCESS FOR REDUCING ALDEHYDES OR KETONES

2. Technical Field:

5 The present invention relates to a new advantageous process for reducing an aldehyde or ketone into a corresponding alcohol with isopropyl alcohol in the presence of a catalyst.

3. Background Art:

10 When an aldehyde or ketone is treated with a metal alkoxide and an alcohol, reduction occurs to form an alcohol corresponding to the aldehyde or ketone. This reaction is well known and it is usually called "Meerwein-Ponndorf reduction" (cf. A.L. Wilds, Org. React., 2, 178 (1944)). Various combinations of a metal alcoholate with an alcohol have been investigated heretofore. Among them, a combination of aluminum isopropoxide with isopropyl alcohol is employed usually, since side reactions such as aldol condensation scarcely occur in the presence thereof, it is soluble not only in alcohols but also in hydrocarbons to make a homogeneous reaction possible and the reaction proceeds rapidly in the presence thereof to form a reduction product usually in a high yield. In this reaction, 25 hydrogen atoms are directly transferred from the alcohol

into the carbonyl group of the aldehyde or ketone
in the presence of aluminum and aluminum isopropoxide
acts as the catalyst. This combination can be employed
in the reduction of several milligrams to several
5 hundred grams of an aldehyde or ketone, since the
reaction system is simple, the reactants are relatively
safe and inexpensive and the reaction proceeds under
mild conditions.

However, since the reaction in the conventional
10 process is a homogeneous reaction, troublesome operations
such as hydrolysis, extraction with an organic solvent,
dehydration and distillation are necessitated for
isolating the product after completion of the reaction.
Further, since the carbonyl group is converted into
15 the hydroxyl group, the product has an increased hydro-
philic property and, therefore, a loss thereof in
the extraction from the aqueous phase with an organic
solvent is large. Although aluminum isopropoxide
is active in the form of mainly its trimer, commercially
20 available aluminum isopropoxide or crystalline aluminum
isopropoxide is in the form of its tetramer having
a low reactivity. Under these circumstances, it is
recommended that the catalyst is prepared immediately
before use in the reduction.
25 In addition, the catalyst must be stored carefully,

since it is gradually hydrolyzed by water in air to form the alcohol and aluminum hydroxide. After completion of the reaction, the catalyst is hydrolyzed so as to isolate the product from the reaction system.

5. The process has a problem that the catalyst cannot, therefore, be used repeatedly and is discharged wastefully.

4. Disclosure of Invention:

An object of the present invention is to provide a catalyst which is stable, highly active and insoluble 10 in a solvent, which can be removed easily from the reaction system after completion of the reaction and which can be used repeatedly.

The present invention provides a process for reducing an aldehyde or ketone characterized in that 15 hydrous zirconium oxide is used in place of a metal alcoholate (mostly aluminum isopropoxide) used heretofore. The inventors were interested in the fact that alcohols are adsorbed to stable hydrous zirconium oxide and, after investigations, the inventors have found that 20 the hydroxyl group of the hydrous zirconium oxide is converted into an alkoxyl group. The present invention has been completed on the basis of this finding.

According to the reduction process of the present invention, an aldehyde or ketone is converted into 25 a corresponding alcohol in a high yield while by-products

are formed in only a small amount. Particularly,
in a liquid phase reaction, a product having a suffi-
ciently high purity can be obtained by merely filtering
off the hydrous zirconium oxide and distilling off
5 the solvent. In a gas phase reaction, the reaction
can be conducted either continuously or batchwise
and the product can be isolated easily in the same
manner as in the liquid-phase reaction.

Hydrous zirconium oxide can be used advantageously,
10 since it necessitates no pretreatment before the reac-
tion, it is insoluble not only in water but also in
organic solvents to make the repeated use after recovery
possible and, therefore, no industrial waste is formed.

5. Best Mode for Carrying Out the Invention:

15 Hydrous zirconium oxide to be used in the present
invention can be produced at a low cost from zircon
sand or baddeleyite present in a large amount as mineral
sources on the earth via zirconium oxychloride ($ZrOCl_2 \cdot 8H_2O$). More particularly, when an aqueous alkali
20 solution is added gradually to an aqueous zirconium
oxychloride solution, the zirconium oxychloride is decomposed
to precipitate a microgel of hydrous zirconium oxide.
The pH of the reaction system is adjusted to 6 to
25 7 and the reaction mixture is filtered to remove an
aqueous solution of excessive acids. As a result,

the microgel is converted into an elastic mass of
the gel. The gel is washed with deionized water,
cut into pieces of a suitable size, spread on a glass
plate and air-dried to form translucent white hard
5 amorphous product. This product is stable in water,
alcohol and many other solvents and is ion-exchangeable
with various metal ions. Alcohols are adsorbed to the
amorphous product. The obtained hydrous zirconium
oxide is dried by heating at about 80°C under reduced
10 pressure and classified to obtain a reaction catalyst.

The reaction may be regarded as conducted in the
similar manner as in a known process for the reduction of
an aldehyde or ketone in liquid phase with a metal alkoxide
and an alcohol except that the metal alkoxide is replaced
15 with hydrous zirconium oxide. Techniques ordinarily
employed in the known process such as distillation
of acetone, i.e. by-product, so as to complete the
reaction rapidly can be employed in the process of
the present invention. In conducting the reaction,
20 hydrous zirconium oxide is added in an amount of 0.1
to 10 g, preferably 1 to 3 g, per mmol of the aldehyde
or ketone, to 0.5 to 10 ml, preferably 1 to 3 ml,
of isopropyl alcohol and the mixture is heated. It
is preferred in accelerating the reaction to distill
25 by-product acetone in the course of the reaction.

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After completion of the reaction, hydrous zirconium oxide is removed by filtration and the filtrate is distilled as it is or, alternatively, the solvent is distilled off to form crystals of the intended product. The used hydrous zirconium oxide is washed with ethanol and then with water to remove powders therefrom and dried to recover hydrous zirconium oxide ready for reuse.

Hydrous zirconium oxide which is in a highly active, stable hard amorphous form can be used also in a gas-phase reaction. In this case, a reaction tube packed with hydrous zirconium oxide is heated to 70 to 200°C, preferably 75 to 110°C and then isopropyl alcohol and an aldehyde or ketone gasified by heating are continuously fed thereinto together with a carrier gas such as air, nitrogen, helium or argon.

The outlet of the reaction tube is cooled with a refrigerant such as water or ice to condense the product, and unreacted isopropyl alcohol and acetone. The product can be isolated in the same manner as in the above-mentioned liquid-phase reaction.

The following examples will further illustrate the present invention, which by no means limit the invention, since various modifications are possible without departing from the gist of the invention.

Example 1

200 g of zirconium oxychloride (octahydrate) was dissolved in 10 l of deionized water. The pH of the solution was adjusted to 6.80 by slowly adding 5 1 N aqueous sodium hydroxide solution under stirring. A hydrate gel thus formed was filtered to separate an aqueous solution of excess salts. The gel was washed with deionized water repeatedly until chloride ion was no more detected in the wash water.

10 The gel was cut into small pieces with a knife, spread on a glass plate and dried to obtain 90 g of hydrous zirconium oxide. A 14- to 20-mesh fraction of the obtained hydrous zirconium oxide dried at 80°C under reduced pressure for 1 h. 10 g of the dried product

15 was taken up and placed in a 100-ml flask provided with a reflux condenser together with 10 ml of isopropyl alcohol and 911 mg (5 mmol) of benzophenone and refluxed gently. The reaction procedure was followed up according to gas chromatography. 53 % of the starting material

20 disappeared after 3 h and 100 % thereof disappeared after 10 h. A peak of the corresponding alcohol was observed. The reaction mixture was cooled to room temperature and filtered through a glass filter (G 3).

Hydrous zirconium oxide was washed thoroughly with 25 ethanol. The filtrate was combined with the washing

and the solvents were distilled off therefrom in a rotary evaporator to obtain crude crystals. After recrystallization from petroleum ether, 905 mg of acicular crystals were obtained. Yield: 98 %.

- 5 Recovered hydrous zirconium oxide was washed thoroughly with hot ethanol on a glass filter (G 3), transferred into a 500-ml beaker and washed with water. Fine suspending material was removed by decantation and the residue was filtered. After air-drying at
10 room temperature followed by heat treatment conducted at 80°C under reduced pressure for 1 h, 9.8 g of hydrous zirconium oxide was obtained in the form of a white translucent amorphous substance. Fresh hydrous zirconium oxide was supplied thereto to a total amount of 10 g.
15 It was used again in the reduction of benzophenone to obtain a reduction product in a yield of 97 %.

Example 2

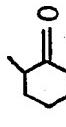
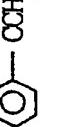
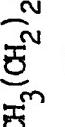
- 10 g of hydrous zirconium oxide dried at 80°C under reduced pressure for 1 h, 5 mmol of an aldehyde or ketone and 10 ml of isopropyl alcohol were placed in a 100-ml flask provided with a reflux condenser and heated under gentle reflux. The progress of the reaction was followed up by subjecting a portion of the reaction solution directly to gas chromatography.
25 After completion of the reaction, hydrous zirconium

oxide was recovered by filtration and washed with 5 ml of isopropyl alcohol or ethanol. The filtrate was combined with the washing and the solvents were distilled off. The residue comprised a substantially 5 pure product. If necessary, the product was purified by distillation or crystallization.

Table 1

<u>Aldehyde or ketone</u>	<u>Reaction time (h)</u>	<u>Reaction product</u>	<u>Yield according to gas chromatography (%)</u>	<u>Per-pass yield (%)</u>
1. $\begin{array}{c} \text{CH}_3 \\ \\ \text{CH}_3\text{CH}_2\text{C}\text{HCHO} \end{array}$	1	$\begin{array}{c} \text{CH}_3 \\ \\ \text{CH}_3\text{CH}_2\text{CHCH}_2\text{OH} \end{array}$	100	-
2. $\text{CH}_3(\text{CH}_2)_4\text{CHO}$	1	$\text{CH}_3(\text{CH}_2)_5\text{OH}$	83	79
3. $\text{CH}_3(\text{CH}_2)_8\text{CHO}$	1.5	$\text{CH}_3(\text{CH}_2)_9\text{OH}$	72	70
4. $\text{C}_6\text{H}_5\text{CHO}$	1	$\text{C}_6\text{H}_5\text{CH}_2\text{OH}$	43	42
5. $\begin{array}{c} \text{CH}_3 \\ \\ \text{C}_6\text{H}_5\text{CH}_2\text{C}\text{HCHO} \end{array}$	5	$\begin{array}{c} \text{CH}_3 \\ \\ >\text{C}_6\text{H}_5\text{CH}_2\text{CH}_2\text{OH} \end{array}$	88	87
6. $\text{C}_6\text{H}_5=\text{O}$	2	$\text{C}_6\text{H}_5\text{CH}_2\text{OH}$	98	96
7. $\text{C}_6\text{H}_5\text{COCH}_3$	12	$\begin{array}{c} \text{OH} \\ \\ \text{C}_6\text{H}_5\text{CH}_2\text{CH}_2\text{OH} \end{array}$	100	98
8. $\text{CH}_3(\text{CH}_2)_6\text{CCH}_2\text{CH}_3$	24	$\text{CH}_3(\text{CH}_2)_6\text{CHCH}_2\text{CH}_3$	100	98
9. $\text{CH}_3(\text{CH}_2)_3\text{CCH}_3$	0	$\begin{array}{c} \text{OH} \\ \\ \text{CH}_3(\text{CH}_2)_3\text{CHCH}_3 \end{array}$	100	94

Table 1 (continued)

<u>Aldehyde or ketone</u>	<u>Reaction time (h)</u>	<u>Reaction product</u>	<u>Yield according to gas chromatography (%)</u>	<u>Per-pass yield (%)</u>
10. 	2		100	95
11. $\text{CH}_3\text{CH}_2\text{CCH}_2\text{CH}_3$	10	$\text{CH}_3\text{CH}_2\text{CCH}_2\text{CH}_3$	100	-
12. 	1		100	100
13. 	10		100	96
14. $\text{CH}_3(\text{CH}_2)_2\text{CHO}$	1	$\text{CH}_3(\text{CH}_2)_3\text{OH}$	80	-
15. $\text{CH}_3\overset{\text{CH}_3}{\underset{ }{\text{CHCHO}}}$	1	$\text{CH}_3\text{CHCH}_2\text{OH}$	100	-

The kind of the aldehyde or ketone, reaction time, reaction product and yield are shown in Table 1.

Example 3

1 g of hydrous zirconium oxide (14- to 20-mesh) 5 was placed in a glass tube having an inner diameter of 4 mm and both ends of the tube were stopped with quartz wool to form a catalyst bed. The catalyst bed portion of the glass tube was placed in a constant-temperature bath kept at 90°C and the inlet and outlet portions thereof were arranged so that they could be heated with a ribbon heater to prevent the reactants and the product from condensing. Nitrogen gas passed through isopropyl alcohol heated to 70°C was introduced thereinto through the inlet. After leaving the tube 10 to stand for 1 h, nitrogen gas passed through cyclohexanone heated to 120°C was also introduced thereinto. The flow rate was 30 ml/min. A given amount of the product was taken at the outlet and its composition was examined according to gas chromatography to reveal that the 15 conversion and the selectivity were both 100 % in a stationary state.

Example 4

1 g of hydrous zirconium oxide (14- to 20-mesh) 20 was placed in a glass tube having an inner diameter of 4 mm and both ends of the tube were stopped with

quartz wool to form a catalyst bed. The catalyst bed portion of the glass tube was placed in a constant-temperature bath kept at 90°C and the inlet and outlet portions thereof were arranged so that they could
5 be heated with a ribbon heater to prevent the reactants and the product from condensing. Nitrogen gas passed through isopropyl alcohol heated to 70°C was introduced thereinto through the inlet. After leaving the tube to stand for 1 h, 2 mmol (379 µl) of 3-decanone was
10 injected thereinto through the inlet by means of a syringe. The flow rate determined at the outlet was 37.5 ml/min. When the total amount of the liquid thus obtained reached 25 ml, the elution of substances other than isopropyl alcohol was no more recognized.
15 According to gas chromatography, the yield of 3-decanol, the intended product, was 97 % and unreacted 3-decanone was not recognized.

WHAT IS CLAIMED IS:

1. A process for reducing an aldehyde or ketone characterized in that an aldehyde or ketone having a carbonyl group is reacted with an alcohol in the presence of hydrous zirconium oxide as a catalyst.
2. A process for reducing an aldehyde or ketone according to Claim 1 wherein the alcohol to be reacted with the aldehyde or ketone is isopropyl alcohol.
3. A process for reducing an aldehyde or ketone according to Claim 1 wherein the reaction of the aldehyde or ketone with the alcohol is a liquid-phase reaction.
4. A process for reducing an aldehyde or ketone according to Claim 1 wherein the reaction of the aldehyde or ketone with the alcohol is a gas-phase reaction.

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WHAT IS CLAIMED IS:

1. (amended) A process for reducing an aldehyde or ketone into an alcohol characterized in that the aldehyde or ketone is reacted with an alcohol in the presence of a solid prepared by partially dehydrating zirconium hydroxide to directly reduce the aldehyde or ketone into a corresponding alcohol.
- 5 2. (amended) A process for reducing an aldehyde or ketone into an alcohol according to Claim 1 wherein the alcohol to be reacted with the aldehyde or ketone is isopropyl alcohol.
- 10 3. (deleted)
4. (amended) A process for reducing an aldehyde or ketone into an alcohol according to Claim 1 wherein direct reduction of the aldehyde or ketone into the alcohol is a liquid-phase reaction or gas-phase reaction.
- 15 5. (added) A process for reducing an aldehyde or ketone into an alcohol according to Claim 1 wherein the reduction of the aldehyde or ketone into the alcohol necessitates no procedure of hydrolysis.
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INTERNATIONAL SEARCH REPORT

International Application No. PCT/JP86/00460

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) ³		
According to International Patent Classification (IPC) or to both National Classification and IPC		
Int.Cl ⁴ C07C29/136, 31/02, 33/20, 35/08, 37/07, 39/08, B01J21/06		
II. FIELDS SEARCHED		
Minimum Documentation Searched ⁵		
Classification System	Classification Symbols	
IPC	C07C29/136-14, 31/00-137, 33/18-24, 35/00-44, 37/06-07, 39/08	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched ⁶		
III. DOCUMENTS CONSIDERED TO BE RELEVANT¹⁴		
Category ⁷	Citation of Document. ¹⁵ with indication, where appropriate, of the relevant passages ¹⁶	Relevant to Claim No. ¹⁴
Y	Indian Journal of Chemistry, Vol. 11, No.8 (1973), p.814-816	1-4
Y	Journal of Organic Chemistry, Vol.51, No.2 (1986), p.240-242	1-4
Y	Collection of Czechoslovak Chemical Communications, Vol.45, No.7, (1980), p.1937-1939	1-4
<p>* Special categories of cited documents:</p> <ul style="list-style-type: none"> "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance: the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance: the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art</p> <p>"&" document member of the same patent family</p>		
IV. CERTIFICATION		
Date of the Actual Completion of the International Search ¹⁷	Date of Mailing of this International Search Report ¹⁸	
November 20, 1986 (20.11.86)	December 8, 1986 (08.12.86)	
International Searching Authority ¹⁹	Signature of Authorized Officer ²⁰	
Japanese Patent Office		

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